



RHEOLOGY

Lecture by
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Physical Pharmacy- 2nd course

Mustansiriyah University/ College of pharmacy



Liquids

Solids

The term rheology, comes from the Greek rheo ("to flow") and logos ("science").

Rheology is used to describe the **flow of liquids and the deformation of solids.**

Viscosity is an expression of the **resistance of a fluid to flow**; the higher the viscosity, the greater is the resistance.

Note:

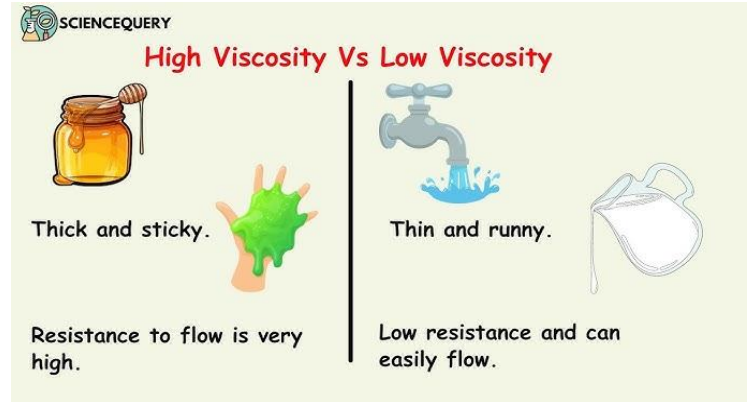
1. **Simple liquids** described in terms of **absolute viscosity** (single value).
2. **Heterogeneous dispersions** rheologic properties are more complex, however, and **cannot be expressed by a single value.**

- **Manufacturers of medicinal and cosmetic creams, pastes, and lotions** must be capable of **producing products with acceptable consistency and smoothness.**
- Valuable information can be obtained by use of analytic methods of rheology, for formulating better pharmaceutical products.
- The **rheology** of product can **affect patient acceptability, physical stability, and even biologic availability.**
- **Rheologic properties** of a pharmaceutical system can **influence the selection of processing equipment.**



Application in pharmacy

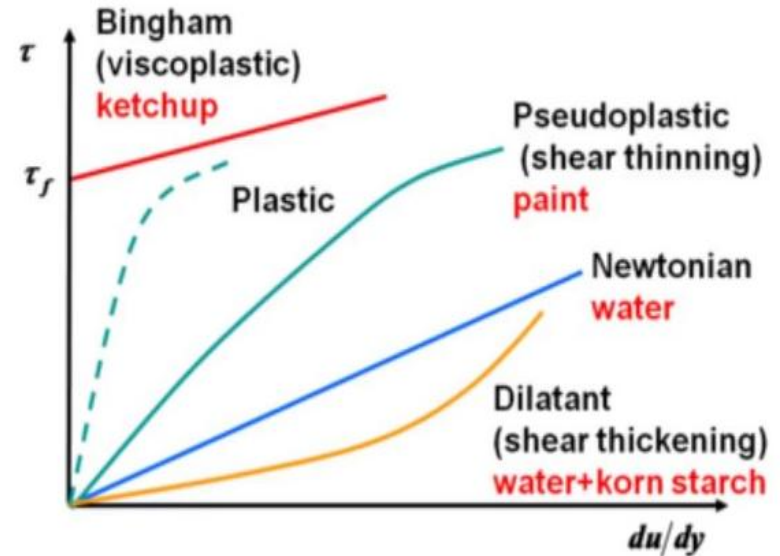
- Formulation of emulsion, paste, suppository and tablet coating.
- Mixing and flow of the material during packaging into container and removal prior usage. Such pouring from a bottle, extrusion from tube, passage through needle.
- Patient acceptance.
- Physical stability.
- Biological availability (absorption rate from GIT)



Classes of materials according to types of flow:

1. Newtonian systems

2. Non-Newtonian systems.



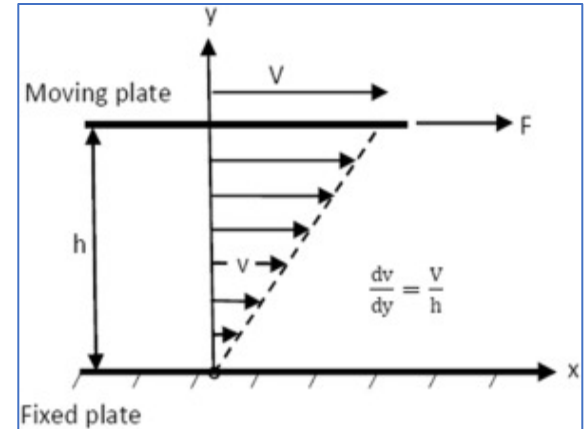
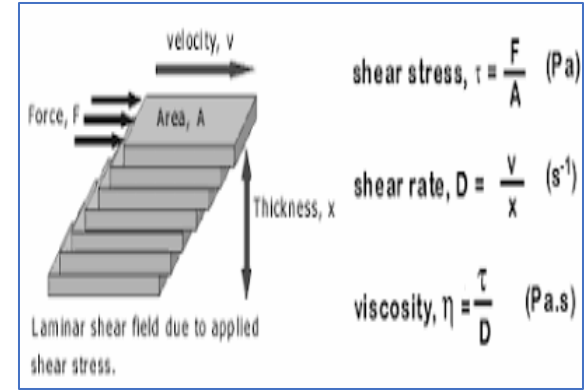
NEWTONIAN SYSTEMS

Newton's Law of Flow

- The higher the viscosity of a liquid, the greater is the force per unit area (shearing stress) required to produce a certain rate of shear”

Shearing force

- A shearing force is applied to the top of the rectangle while the bottom is held in place. The resulting shear stress, F , deforms the rectangle into a parallelogram متوازي الاضلاع. The area involved would be the top of the parallelogram.

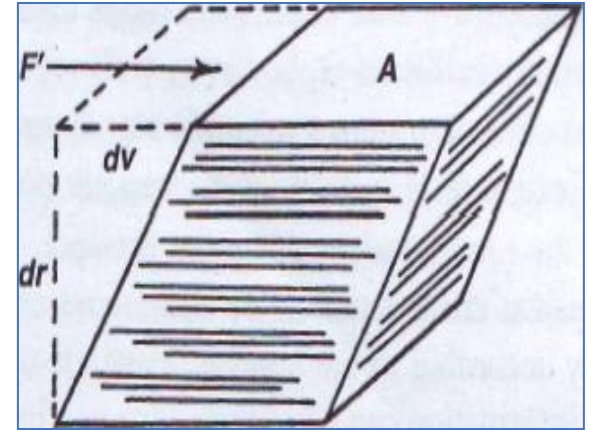


Rate of shear or the velocity gradient: $\left(\frac{dv}{dr}\right)=G$

- Is the difference of velocity, dv , between two planes of liquid separated by an infinitesimal متناهي الصغر distance dr .

Shearing stress : $\left(\frac{F'}{A}\right)=F$

- Is the force per unit area required to bring about flow.



- Newton was recognized that the higher the viscosity of a liquid, the greater is the force per unit area (shearing stress) required to produce a certain rate of shear. Hence, rate of shear should be directly proportional to shearing stress, or

$$\frac{F'}{A} = \eta \frac{dv}{dr}$$

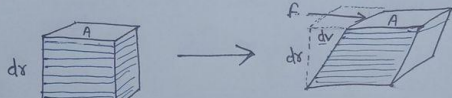
Where, η is the coefficient of viscosity, usually referred to simply as viscosity.

Above equation is frequently written as

$$\eta = \frac{F}{G}$$

where, $F = F'/A$ and $G = dv/dr$.

→ NEWTON LAW OF FLOW
 IN A FLUID RATE OF SHEAR IS DIRECTLY
 PROPORTIONAL TO SHEARING STRESS



SHEARING STRESS = $\frac{F}{A}$

RATE OF SHEAR = $\frac{dv}{dx}$

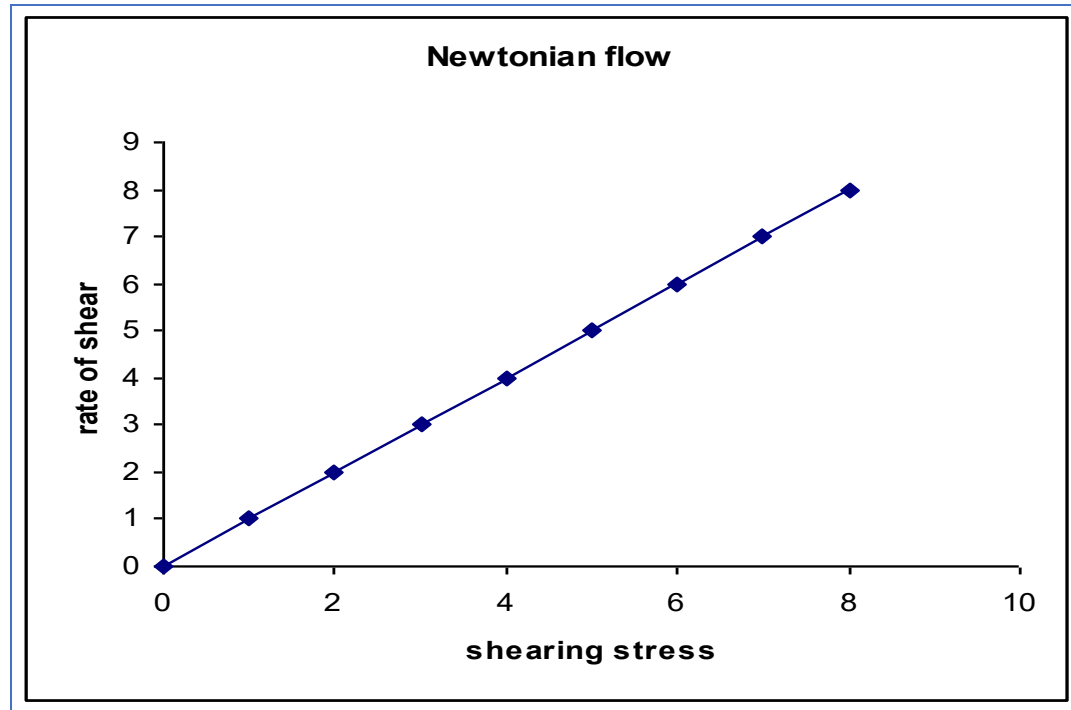
∴ SHEARING STRESS ∝ RATE OF SHEAR

$\frac{F}{A} \propto \frac{dv}{dx}$

$\frac{F}{A} = \eta \frac{dv}{dx}$ $\eta = \text{VISCOSITY}$

NEWTONIAN FLUIDS — OBEY NEWTONS LAW OF FLOW
 NON NEWTONIAN FLUIDS — DO NOT OBEY

- A representative flow curve, or rheogram, obtained by plotting F versus G for a Newtonian system is shown in this figure.



- The **unit of viscosity is the poise**, defined as the shearing force required to produce a velocity of 1 cm/sec between two parallel planes of liquid each 1 cm² in area and separated by a distance of 1 cm. The units for **poise are dyne sec cm⁻²** (i.e., dyne sec/cm²) or **g cm⁻¹ sec⁻¹** (i.e., g/cm sec).
- A more convenient unit for most work is the centipoise (cp), 1 cp being equal to 0.01 poise.

Fluidity, ϕ , a term sometimes used, is defined as the **reciprocal of viscosity** (**Defines also as the ability to flow**)

$$\phi = \frac{1}{\eta}$$

Kinematic Viscosity

Kinematic viscosity is the **absolute viscosity divided by the density of the liquid at a specific temperature** (**measure of a fluid's resistance to flow under the influence of gravity**):

$$\text{Kinematic viscosity} = \frac{\eta}{\rho}$$

The units of **kinematic viscosity are the stoke (s) and the centistoke (cs)**.

Absolute viscosities of some Newtonian liquids at 20 C° commonly used in pharmacy are given in this table:

Liquid	Viscosity (cp)
Castor oil	1000
Olive oil	100
Water	1.0019

Note: Water is ordinarily used as a standard for viscosity of liquids. Its viscosity at 25°C is 0.8904 cp.

Temperature Dependence and the Theory of Viscosity

- The **viscosity of liquid decreases as temperature is raised**, and the **fluidity of a liquid** (the reciprocal of viscosity) **increases with temperature**.
- The dependence of the viscosity of a liquid on temperature is expressed approximately for many substances by an equation analogous to the **Arrhenius equation** of chemical kinetics:

$$\eta = Ae^{E_v/RT}$$

Where A is a constant depending on the molecular weight and molar volume of the liquid and E_v , is "activation energy" required to initiate flow between molecules.

NON-NEWTONIAN SYSTEMS

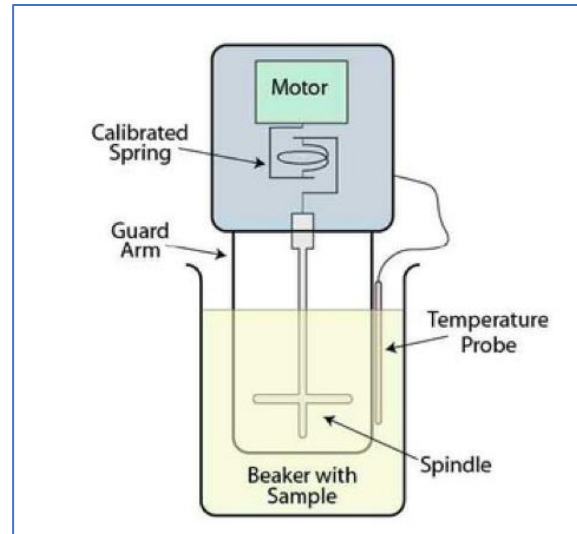
- Most fluid pharmaceutical products are not simple liquids and do not follow Newton's law of flow. These systems are referred to as non-Newtonian.
- **Non-Newtonian behavior is generally exhibited by liquid and solid heterogeneous dispersions such as colloidal solutions, emulsions, liquid suspensions, and ointments.**
- In a **non-Newtonian fluid, the relation** between the **shear stress and the strain rate** is **nonlinear**, and can even be **time-dependent**. Therefore, a constant coefficient of viscosity cannot be defined.
- A ratio between shear stress and rate of strain (or shear-dependent viscosity) can be defined, this concept being more useful for fluids without time-dependent behavior.

When **non-Newtonian materials** are analyzed in a **rotational viscometer** and results are plotted, various consistency curves, representing three classes of flow, are recognized:

1- Plastic

2- Pseudoplastic

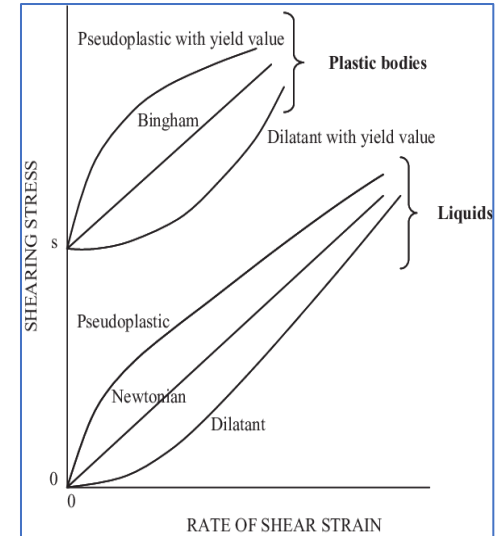
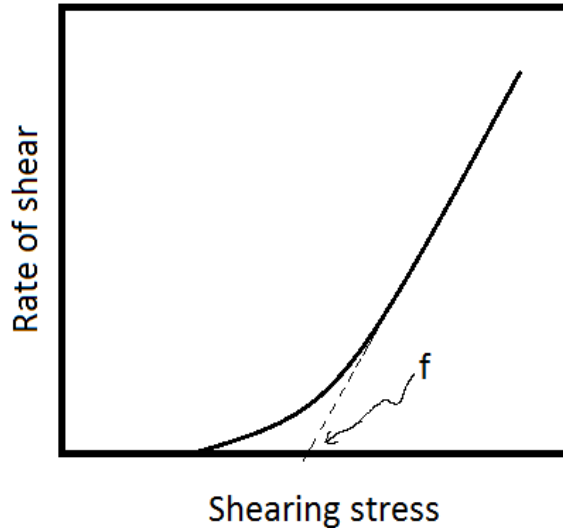
3- Dilatant.



Plastic Flow

- In Figure below, the curve represents a body that exhibits plastic flow; such materials are known as **Bingham bodies** (like clay suspensions, drilling mud, toothpaste, mayonnaise, chocolate, and mustard). **The classic case is ketchup which will not come out of the bottle until you stress it by shaking.**

• **Plastic flow curves do not pass through the origin, but rather intersect the shearing stress axis (or will if the straight part of the curve is extrapolated to the axis) at a particular point referred to as the yield value.**



- A Bingham body does not begin to flow until a shearing stress corresponding to the yield value is exceeded. At stresses below the yield value, the substance acts as an elastic material.
- Yield value is an important property of certain dispersions.
- The slope of the rheogram in the Figure is termed the mobility, analogous to fluidity in Newtonian systems, and its reciprocal is known as the plastic viscosity, U . The equation describing plastic flow is:

$$U = \frac{F-f}{G}$$

Where, f is the yield value, or intercept, on the shear stress axis in dynes/cm².

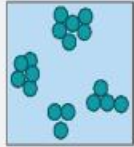




In practice, **deformation and flow** usually **occurs at a lower shear stress value** and this accounts for the **curved portion of the curve**.



- The **viscosity decreases initially** and then remains constant.



• In a highly flocculated system, there is interaction between flocs which results in a structured system and plastic flow that is associated with these systems e.g **highly flocculated suspensions**.



- The **yield value is present because of the contacts between adjacent particles to form network** (flocculation caused by **van der Waals forces** which may be capable of withstanding weak stresses) which must be **broken down before flow can occur**.



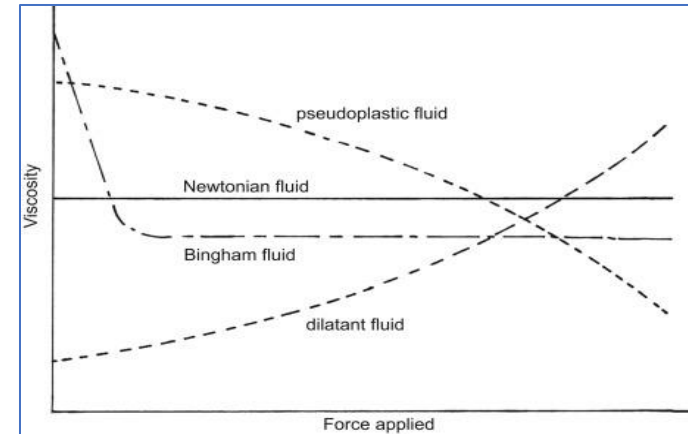
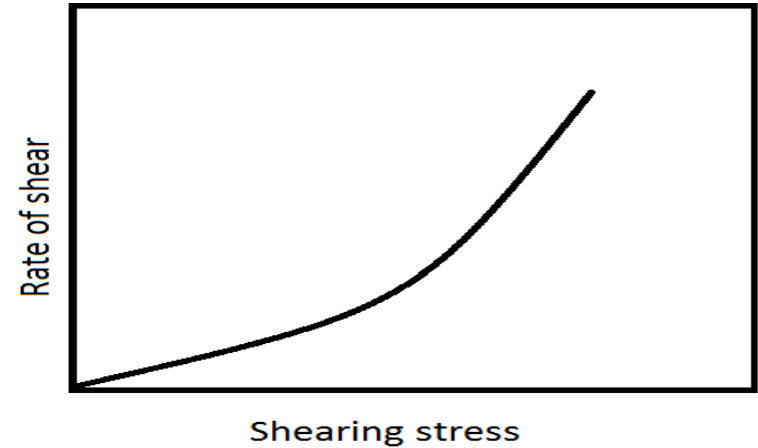
• The **yield value is an indication of the degree of flocculation**; the more flocculated the suspension, the higher will be the yield value (keep flocculated particles suspended, preventing sedimentation). If the yield value is too low, flocs can break apart and settle over time).



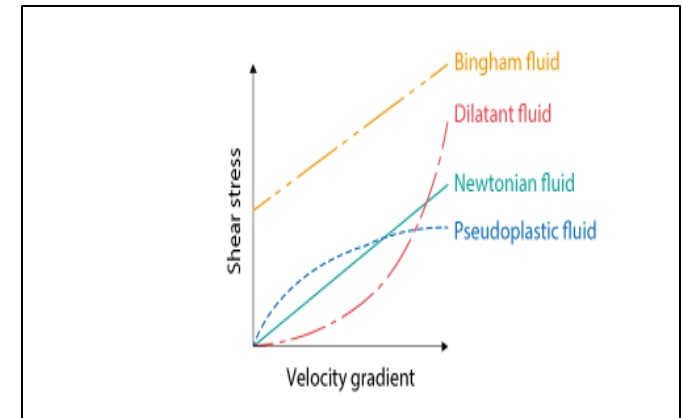
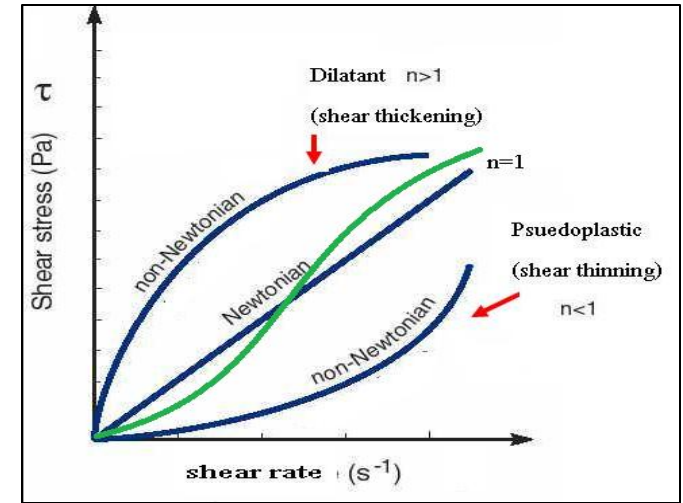
- This type of behaviour is also exhibited by **creams and ointments**.

Pseudoplastic Flow

- Many pharmaceutical products exhibit *pseudoplastic flow* include natural and synthetic gums e.g. liquid dispersions of tragacanth, sodium alginate, methylcellulose, sodium carboxymethylcellulose.
- Pseudoplastic flow is typically exhibited by polymers in solution, in contrast to plastic systems, which are composed of flocculated particles in suspension. As seen in this Figure, the consistency curve for a pseudoplastic material begins at the origin. Therefore, there is no yield value as there is in a plastic system.



- Furthermore, because no part of the curve is linear, the viscosity of a pseudoplastic material cannot be expressed by any single value.
- The viscosity of a pseudoplastic substance decreases with increasing rate of shear (**shear-thinning systems**).
- An apparent viscosity can be obtained at any rate of shear from the slope of the tangent to the curve at the specified point.
- The most satisfactory representation for a pseudoplastic material, however, is probably a graphic plot of the entire consistency curve.
- **Objective comparisons between different pseudoplastic systems are more difficult than with either Newtonian or plastic systems.** For example, **Newtonian systems are completely described by viscosity, η , and plastic systems are adequately described by yield value, f , and plastic viscosity, U .**



However, the exponential formula can be used to compare rheology of pseudoplastic materials to be compared.

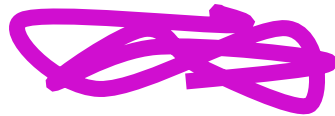
$$F^N = \eta' G$$

The exponent N rises as flow becomes increasingly non-Newtonian.

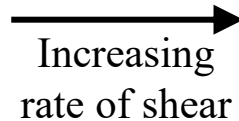
When $N = 1$, the equation reduces to equation ($\eta = \frac{F}{G}$) and flow is Newtonian. The term η' is a viscosity coefficient.

At the Particulate level:

- The **curved rheogram for pseudoplastic materials results from a shearing action on the long-chain molecules** which become entangled and associated with immobilized solvent.
 - As the **shearing stress is increased**, the randomly arranged particles tend to become disentangled and align their long axes in the direction of flow.
- ↓
- This orientation **reduces the internal resistance of the material and offers less resistance to flow**. Some of the entrapped water will also be released.
- ↓
- Both of these account for the **lower viscosity**. Once stress is removed, the structures reform spontaneously.



Coiled polymer at rest



Linear polymer at increased shear stress

Dilatant Flow

If suspensions with a high percentage of dispersed solids (>50%)

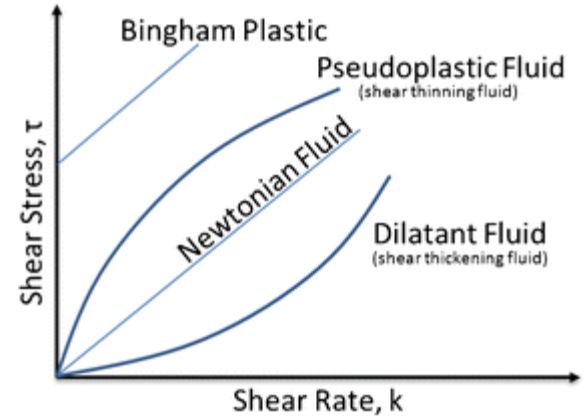


Exhibit an increase in resistance to flow with increasing rates of shear.



Such systems increase in volume when sheared and are hence termed **dilatant**.

Figures illustrates their flow properties:



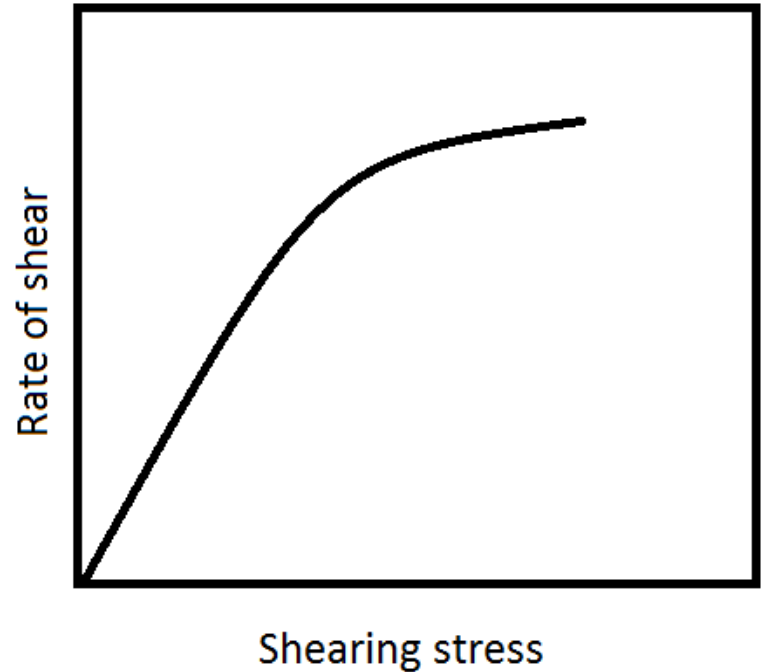
- Dilatant flow is the inverse of that possessed by pseudoplastic systems.

- **Pseudoplastic materials** are termed "shear-thinning systems".

- **Dilatant materials** are termed "shear-thickening systems".



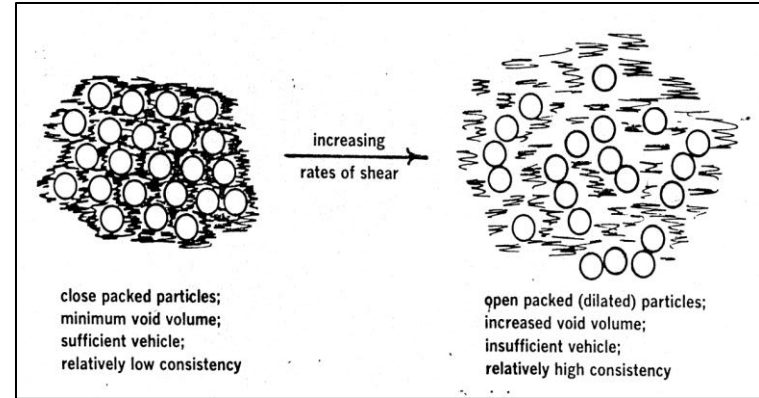
When stress is removed, a dilatant system returns to its original state of fluidity.



At the particulate level:

At rest:

- **Particles:**
 - closely packed
 - voids at a minimum.
- **Vehicle:**
 - sufficient to fill this volume
 - allows the particles to move relative to one another at low rates of shear.
- **Can pour a dilatant suspension from a bottle without shaking as it is relatively fluid without shear stress applied.**



At stress:

- If the shear stress is increased by shaking
↓
- Bulk expands or dilates
↓
- Particles move quickly past each other and take an open form of packing.

Mechanism:

- Such an arrangement (Shaking) → significant increase in the void volume



vehicle now being insufficient to fill the voids between the particles.



The **resistance to flow increases** since the (particles are no longer completely wetted or lubricated by the vehicle) and eventually the **suspension will set up as a firm paste.**

Caution must be taken in processing dilatant materials.

- Usually, the processing of dispersions containing solid particles is facilitated using high-speed mixers, blenders or mills.



Dilatant materials may solidify under these conditions of high shear, thereby overloading and damaging the processing equipment. (whipping cream)

- <https://youtu.be/E4n4AqjPKVo>

- Equation ($F^N = \eta' G$)

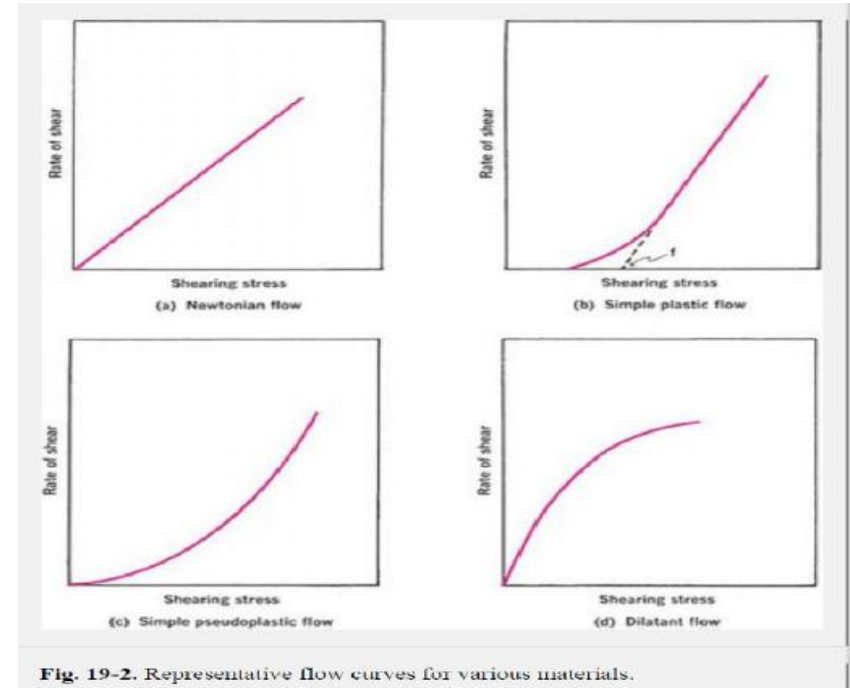
Used to describe dilatancy in quantitative terms.

- Always $N < 1$

N decreases as degree of dilatancy increases meaning viscosity rises sharply with shear rate.

- As $N=1$, the system becomes increasingly Newtonian in behavior.

- Substances possessing dilatant flow properties are invariably (suspensions) containing a high concentration (50% or more) of small, deflocculated particles.



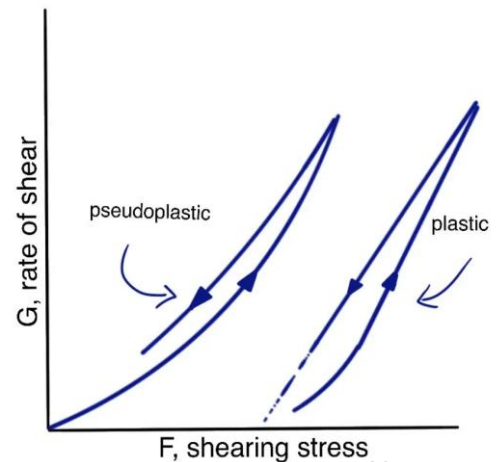
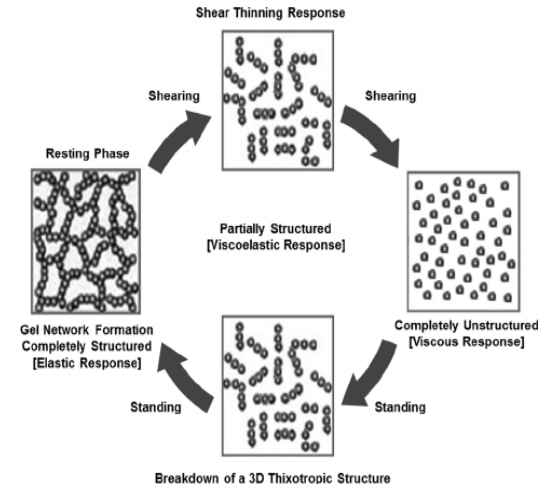
THANK YOU!

THIXOTROPY

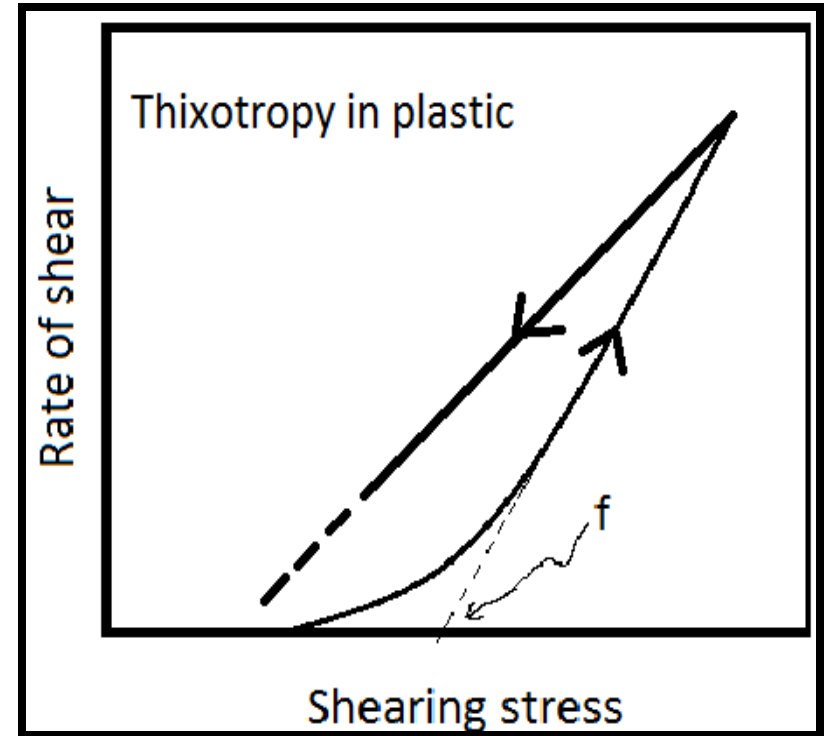
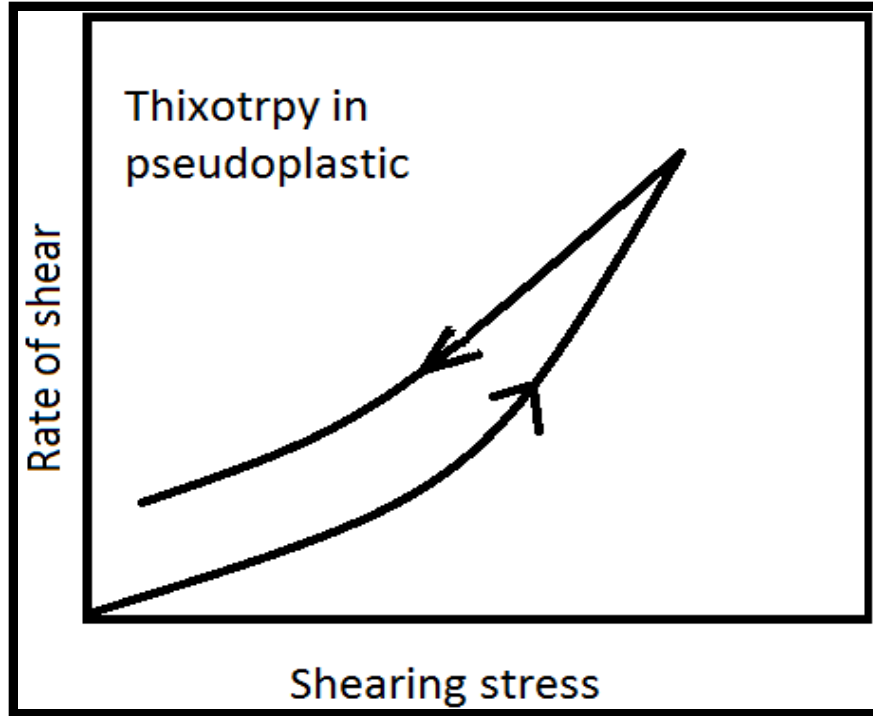
- Several types of behavior are observed when rate of shear is progressively increased and plotted against resulting shear stress.
- If this had been reached, and **rate of shear were reduced when the maximum the resulted down curve is identical with the upcurve**, this system is **Newtonian systems**.
- With **shear-thinning systems (i.e., pseudoplastic)**, the **down-curve is frequently displaced to the left of the up-curve** (Figure), showing that the material has a lower consistency at the down-curve than at upcurve.
- This phenomenon, known as **thixotropy**, can be defined as "**an isothermal** (constant temp.) and comparatively **slow recovery**, on standing of a material, of a **consistency lost through shearing.**"

Summarize

- **At rest**, the fluid has a **structured network** that holds it together.
- When shear is applied (stirring or shaking), the structure **breaks down**, causing viscosity to drop.
- Once the shear stops, the structure **slowly rebuilds**, and viscosity increases again.



Typical rheograms for plastic and pseudoplastic systems exhibiting this behavior are shown in the following Figure.



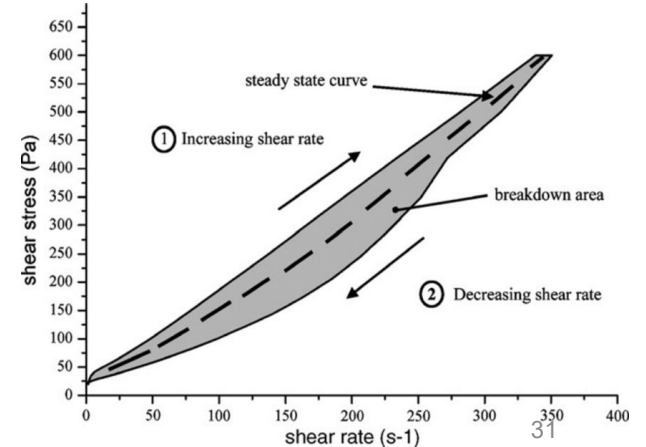
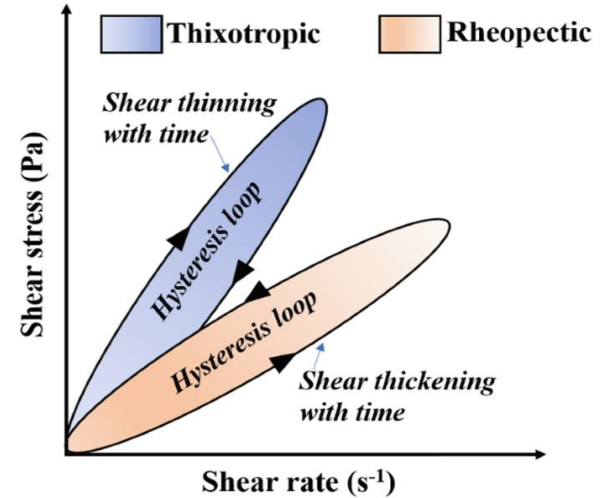
An important point to obtain a **quantitative measure** of thixotropy:

Rheograms obtained with thixotropic materials (same product) is **different and highly dependent on:**

- 1- **shear rate** (increased or decreased)
- 2- **length of time** a sample is subjected to rate of shear.
- 3- **degree of structure** in the sample.

Hysteresis loop: Is the **area between the upcurve and downcurve of rheogram.**

•A **thixotropic hysteresis loop** can be obtained by measuring the **non-equilibrium shear stress** as a shear rate is first increased and then decreased in standard way.



Examples:

1. Solutions of high polymers (thixotropic to a certain extent) **intermolecular attractions**.
e.g. sols of iron(III)oxide , alumina and many clay.
2. In paint industry [the **paint should flow only when being brushed on to appropriate surface (high rate of shear)**] and immediately after brushing.

Properties of thixotropic systems: usually **contain a symmetric particles** that **through numerous point of contact, set up a loose 3D network** throughout the sample.

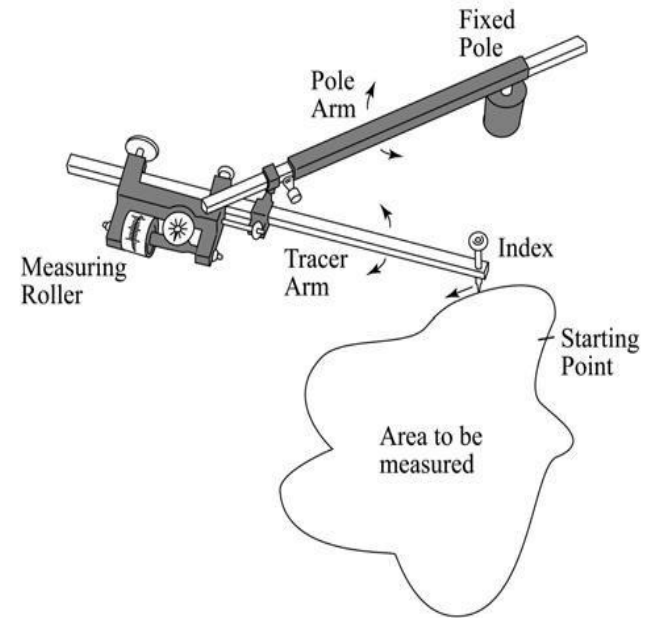
Mechanism:

1. **At rest:** this structure confers some degree of rigidity on the system, and it **resemble a gel**.
2. **As shear is applied:** flow starts **structure beings to break down**, are disrupted and particles become a lined. The material undergoes a **gel-to-sol transformation and exhibits shear thinning**.
3. **On removal of stress:** the **structure starts to reform**.

Measurement of Thixotropy

The area of hysteresis proposed as a measure of thixotropic breakdown.

Instrument: planimeter (is a table-top instrument for measuring areas, usually the areas of irregular regions on a map or photograph).



- **With plastic (Bingham) bodies, two approaches are frequently used to estimate degree of thixotropy:**

First: determine **structural breakdown with time** of a plastic system when subjected to a constant rate of shear (t) (**maximum shear rate is constant, while time of holding before reducing shearing stress is different**).

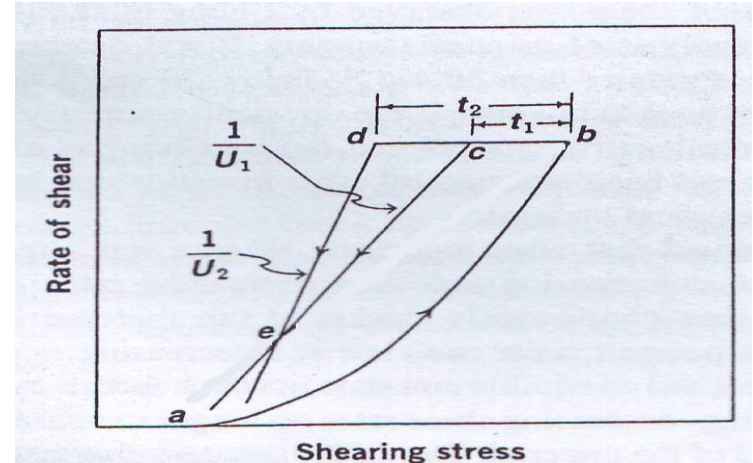
Based on such a rheogram, a **thixotropic coefficient (B)**: the **rate of breakdown with time at constant shear rate**, is calculated as follows:

Indication: represents how fast the viscosity decreases with time under shear.

$$B = \frac{U_1 - U_2}{\ln \frac{t_2}{t_1}}$$

More: A higher B value means a faster breakdown of the internal structure.

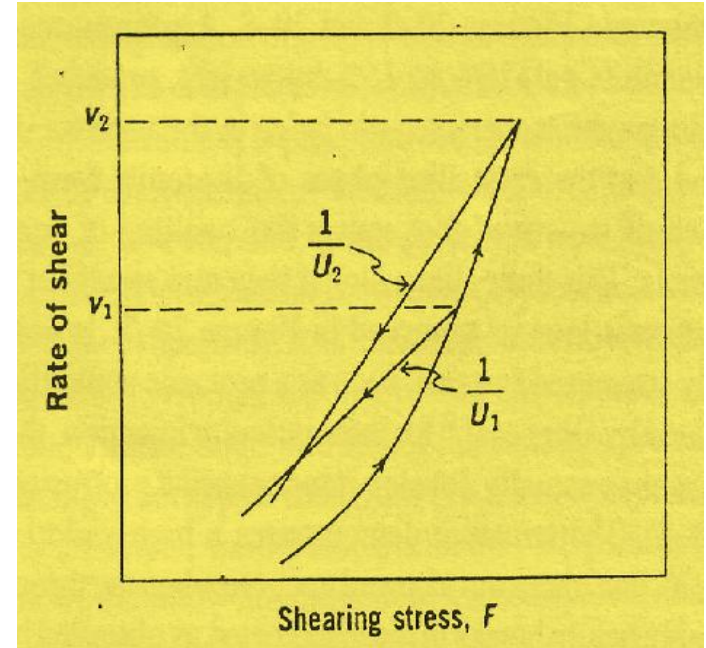
- where U_1 , and U_2 are the **plastic viscosities of the two downcurves**, calculated from equation ($U = \frac{F - f}{G}$),
- After shearing at a constant rate for t_1 and t_2 seconds, respectively.



- **Second:** determine the structural breakdown of a plastic system when subjected to increasing shear rates (V). (The maximum shear rate is different; the time of holding before reducing shearing stress is constant).
- **Principle:** two hysteresis loops are obtained having different maximum rates of shear, v_1 and v_2 . (Larger loop = more breakdown structure)
- In this case, a **thixotropic coefficient (M)** represents the loss in shearing stress per unit increase in shear rate, is obtained from:

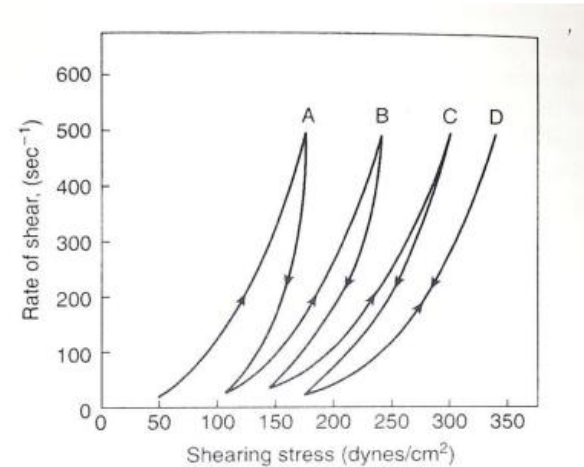
$$M = \frac{U_1 - U_2}{\ln\left(\frac{v_2}{v_1}\right)}$$

where M is in dynes sec/cm² and U_1 , and U_2 are the plastic viscosities for two separate downcurves having maximum shearing rates of v_1 and v_2 , respectively.



Negative Thixotropy or Antithixotropy

- It is phenomenon represents an **increase** rather than a decrease in consistency on the **downcurve (formation of internal structure under stress)**.
- This **increase in thickness with increased time of shear (shear thickening)** in the rheologic analysis: e.g. magnesia magma (**shear rates of greater than 30 sec^{-1}**)
- While (**below 30 sec^{-1}**) the magma showed **normal thixotropy**, the **downcurve appearing to the left of the upcurve**.

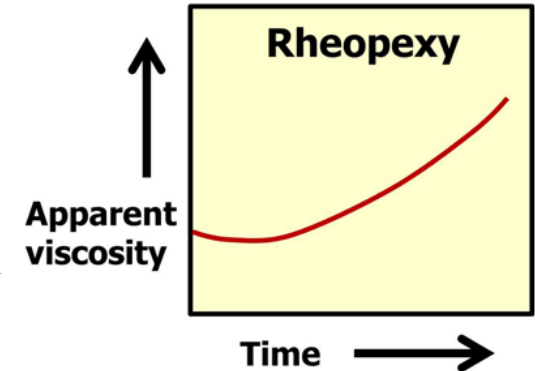
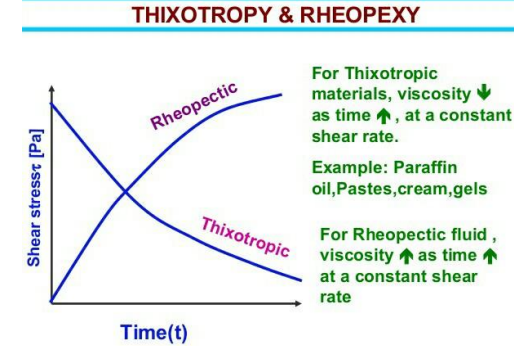


i) Rheogram of magnesia magma showing ant thixotropic behavior.

- Negative thixotropy or antithixotropy should not be confused with dilatancy or rheopexy:

Property	Dilatancy	Antithixotropy
Definition	A shear-thickening behavior where viscosity increases instantly when shear is applied and returns to normal immediately when shear stops.	A time-dependent shear-thickening behavior where viscosity gradually increases under shear and gradually decreases after shear is removed.
Type of system	Deflocculated (Starch in water)	Flocculated (clay suspensions, some gels)
Content	Greater than 50% by volume of solid dispersed phase	Low solids content (1%-10%)
Cause	Increased particle interactions in highly concentrated suspensions (particles move apart, increasing resistance).	Formation of a network structure over time under shear, leading to thickening.
Hysteresis Loop	No hysteresis loop (instantaneous response).	Counterclockwise hysteresis loop (time-dependent response).

- **Rheopexy** is a phenomenon in which solid forms a gel more readily when gently shaken (rolling and rocking motion so particles acquire random orientation and network established) than when allowed to form the gel while the material is kept at rest.
- In a rheoplectic system, the gel is the equilibrium form, whereas in antithixotropy, the equilibrium state is the sol.



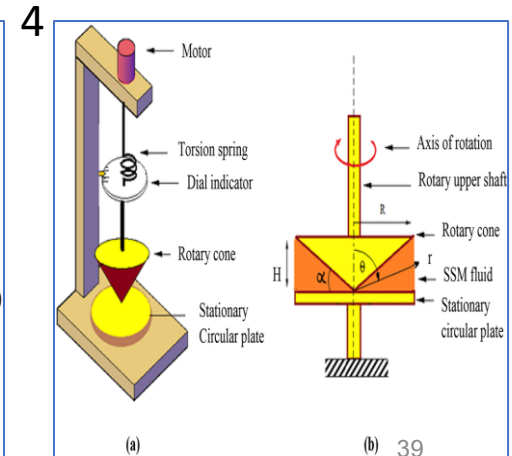
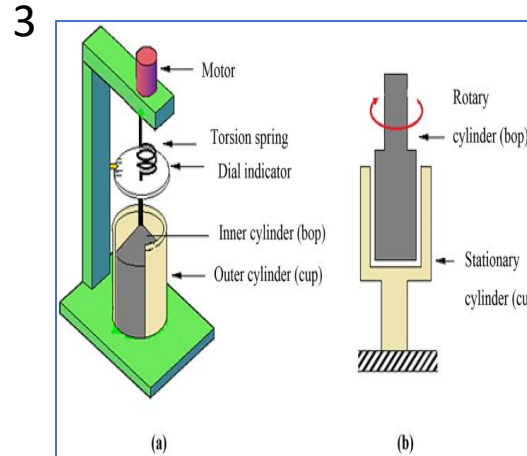
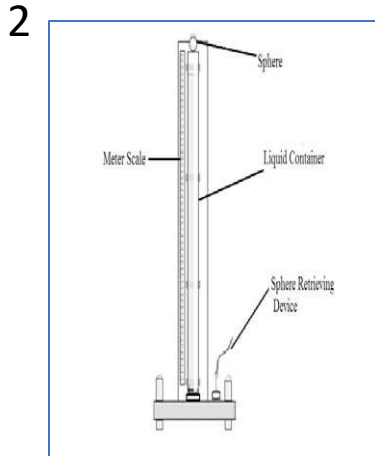
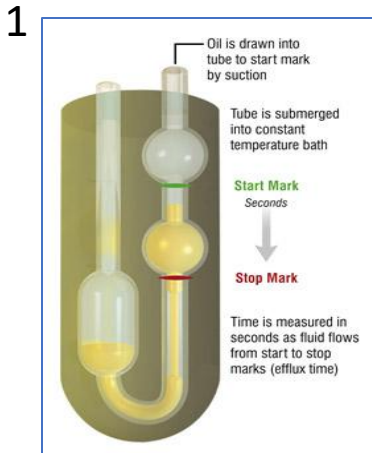
DETERMINATION OF RHEOLOGIC PROPERTIES

➤ Choice of Viscometer

- **Newtonian system:** shear rate is directly proportional to shearing stress, instruments that operate at a single shear rate can be used. These "single-point instruments" provide a single point on the rheogram; extrapolation of a line through this point to the origin will result in a complete rheogram.
- For **Non-Newtonian:** a single-point determination is virtually useless in characterizing its flow properties. It is therefore essential that, with non-Newtonian systems, the instrument can operate at a variety of shear rates. Such "multipoint instruments" are capable of producing a complete rheogram for non-Newtonian systems.

The main instruments used for determination of rheological properties:

- 1- Capillary
 - 2- Falling-sphere
 - 3- Cup-and-bob
 - 4- Cone-and-plate viscometers.
- single-shear-rate instruments suitable for use only with Newtonian materials
- (multipoint, rotational instruments) can be used with both Newtonian and non-Newtonian systems.



VISCOELASTICITY

- Viscoelastic measurements are based on the **mechanical properties of materials** that exhibit both **viscous properties of liquids** and **elastic properties of solids**.
- Many of the systems studied in pharmacy belong to this class, examples being **creams, lotions, ointments, suppositories, suspensions, and the colloidal dispersing, emulsifying, and suspending agents**.

Pharmaceutical areas in which rheology is significant

1. Fluids

- a. **Mixing**
- b. **Particle-size reduction of disperse systems with shear.**
- c. **Passage through orifices** (pouring, packaging in bottles, and passage through hypodermic needles).
- d. **Fluid transfer** (pumping and flow through pipes
- e. **Physical stability of disperse systems**).

2. Quasisolids (semisolids)

- a. Spreading and adherence on the skin.
- b. Removal from jars or extrusion from tubes.
- c. Capacity of solids to mix with miscible liquids.
- d. Release of the drug from the base.

3. Solids

- a. Flow of powders from hoppers and into die cavities in tableting or into capsules during encapsulation.
- b. Packageability of powdered or granular solids.

4. Processing

- a. Production capacity of the equipment.
- b. Processing efficiency.

A top-down view of a desk with a light-colored, wood-grain texture. In the center is a white spiral-bound notebook with the words "THANK YOU!" written in large, bold, black letters. The exclamation point is red. To the top left of the notebook are a pair of gold-rimmed glasses. To the right is a silver and black ballpoint pen. In the bottom left corner is a small white pot containing a green succulent plant. In the bottom right corner, a portion of a black circular object is visible.

**THANK
YOU!**